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Description	



Japan Advanced Institute of Science and Technology

1	Perpendicular Orientation of Dispersed Rubber in an
2	Oriented Polypropylene Sheet
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25	

## 26 Abstract

27	An immiscible blend of isotactic polypropylene (PP) and ethylene-butene-1
28	copolymer (EB) (PP/EB = $70/30$ ) containing a small amount of <i>N</i> , <i>N</i> '-dicyclohexyl-2,6-
29	naphthalenedicarboxamide as a nucleating agent for $\beta$ -form crystals was prepared by T-
30	die extrusion. We successfully prepared an extruded sheet, in which the orientation of the
31	PP molecules is perpendicular to the deformation of the EB particles; i.e., the $\beta$ -form
32	crystals of PP are predominantly oriented perpendicular to the flow direction of the sheet
33	plane (the transverse direction, TD), whereas the EB droplets are strongly deformed in
34	the flow direction. It should be noted that the EB barely affects the crystalline form and
35	orientation of PP. This extraordinary structure provides unique mechanical anisotropy.
36	The tear strength in the TD sample is significantly enhanced with the anomalous crack
37	propagation in the machine direction (MD). Moreover, the anisotropy in tensile properties
38	such as Young's modulus, yield stress, strain at break, and dynamic tensile modulus
39	becomes reduced.
40	
41	Keywords: polypropylene; ethylene-butene-1 copolymer; T-die extrusion; mechanical
42	anisotropy
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#### Introduction

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52 Isotactic polypropylene (PP) is widely used in various applications because it is 53 inexpensive and lightweight. In particular, the trend in the automobile industry to use 54 PP will continue because weight reduction is an inevitable future priority. Generally 55 speaking, both rigidity and high impact strength are required for a material design of PP 56 [1]. Therefore, the technology of the blend with rubber [1-17] and fillers [18,19] and the 57 addition of a nucleating agent [20-25] has been intensively studied. Various types of 58 elastomeric materials have been employed as impact modifiers. In particular, after the 59 development of metallocene catalyst, ethylene-butene-1, ethylene-hexene-1, and 60 ethylene-octene-1 copolymers have been preferred for this purpose, because they have 61 low interfacial tension with PP compared with traditional ethylene-propylene copolymers. 62 Such miscibility and/or compatibility have been predicted by the difference in statistical 63 segment length [1,12,17] and packing length [8,14,17], and have been summarized from 64 the perspective of the species and content of the  $\alpha$ -olefin [2,3,7,15]. The rheological 65 properties [4,5,9], crystallization behavior [6,16], and processability [10,11] of PP blends 66 with ethylene- $\alpha$ -olefin copolymers have also been elucidated. Accordingly, controlling 67 the particle size of a rubber dispersion in a PP continuous phase improves the mechanical 68 properties of the material. In general, low interfacial tension, and viscosity matching 69 between components enable the formation of small particles with uniform dispersion by 70 melt blending. Furthermore, the nucleation process of PP plays a key role in the 71 processing operation because its mechanical properties are largely dependent on the form 72 and degree of crystallinity. As well known, PP has various crystalline forms such as 73 monoclinic  $\alpha$  modification, trigonal  $\beta$  modification, orthorhombic  $\gamma$  modification, and

74 smectic form, which are determined by crystallization conditions and additives 75 [2,3,7,8,12,14,17]. Of all the crystalline structures, recent attention has focused on  $\beta$ -form 76 crystals owing to the development of highly efficient nucleating agents such as 1,3,5-77 benzenetrisamide [26] and N,N'-dicyclohexyl-2,6-naphthalenedicarboxamide [27,28]. 78 These nucleating agents enhance the modulus, which was considered one of the 79 unfavorable properties of  $\beta$ -form crystals. Moreover, a recent report on the enhancement 80 of the melting point using  $\beta$ -form crystals [29] should encourage the industrial 81 applications.

82 N,N'-dicyclohexyl-2,6-naphthalenedicarboxamide has been used to ensure the 83 molecular orientation of the PP chains in the transverse direction (TD) [30-35]. Under 84 suitable processing conditions, the nucleating agent appears as needle-shaped crystals in 85 PP, and is aligned with the direction of flow by hydrodynamic force. Owing to the unique 86 crystallization behavior of PP, in which the *c*-axis of the PP crystals grows perpendicular 87 to the long axis of the needle-shaped nucleating agent by epitaxial crystallization, the PP 88 chains orient perpendicular to the flow direction during T-die extrusion [31]. The resulting 89 product has unique mechanical properties. Orientation control using nucleating agents is 90 applicable to injection-molding. The peculiar orientation of the PP chains, i.e., in a 91 plywood-like structure, prohibits crack propagation and reduces anisotropy in modulus 92 and in thermal expansion [32,35]. A combined approach involving the addition of rubber 93 and the control of orientation using a specific  $\beta$  nucleating agent is expected to maximize 94 the mechanical performance of PP. Although several papers have been published 95 regarding polymer blends of PP and ethylene- $\alpha$ -olefin copolymers, there have been few 96 reports describing in detail of PP blends containing a  $\beta$  nucleating agent [36-39].

97	Furthermore, in industrial applications the molecular orientation of the PP and the rubber
98	dispersion are controlled independently.
99	The present research focuses on an extruded sheet comprising PP and ethylene-
100	butene-1 copolymer (EB) with the nucleating agent, N,N'-dicyclohexyl-2,6-naphthalene-
101	dicarboxamide. The orientation of the PP molecular chains and the deformation direction
102	of the rubber particles are investigated in detail with an evaluation of the mechanical
103	properties.
104	
105	Materials and Methods
106	
107	Materials
108	The raw materials used in the present study were: a commercially available
109	isotactic polypropylene homopolymer (PP) (SunAllomer, PM600A, melt flow rate (MFR)
110	7.5 [g/10 min at 230°C], Mn 63,000, Mw 360,000), and an ethylene-butene-1 copolymer
111	(EB) (Mitsui Chemicals, TAFER DF610, MFR 2.2 [g/10 min at 230°C], density 860
112	kg/m <sup>3</sup> , ethylene content 54 wt.%). N,N'-dicyclohexyl-2,6-naphthalenedicarboxamide
113	(New Japan Chemical, NJ Star NU-100) was used as a $\beta$ nucleating agent without further
114	purification.
115	
116	Sample preparation
117	Melt-mixing of PP with 0.1 wt.% of the $\beta$ nucleating agent was performed by a
118	counter-rotating twin-screw extruder (Technovel, KZW15TW-45MG-NH) with 0.05
119	wt.% of 3-(3,5-di-tert-butyl-4-hydroxyphenyl)propionate (Ciba, Irganox 1010) and 0.1
120	wt.% of tris(2,4-di-tert-butyl-phenyl)phosphate (Ciba, Irgafos 168) as thermal stabilizers,

and 0.05 wt.% of calcium stearate (Nitto Kasei Kogyo) as a neutralizing agent. The screw
diameter of the extruder was 15 mm and the length-to-diameter ratio was 45. The machine
was operated at a screw rotation speed of 250 rpm. The mixing was performed at 260°C
to completely dissolve the nucleating agent in molten PP. The extruded strands were
dipped in a water-bath and cut into pellets approximately 2.3 mm in diameter.

126 The pellets of PP containing the nucleating agent and EB were fed into a single-127 screw extruder (Technovel, SZW25GT-28VG-STD) equipped with a T-die (300 mm wide 128 with a 0.5 mm die lip) at a blend ratio of 70/30 (PP/EB) by weight. The out-put rate was 129 3 kg/h. The screw diameter and the length-to-diameter ratio were 25 mm and 28, 130 respectively. The speed of screw rotation was 40 rpm. The sheet was stretched in the air 131 gap (10 mm) between the die lip and the chill roll. The temperatures of the die and chill 132 roll were maintained at 200°C and 103°C, respectively. The diameter of the chill roll was 133 250 mm and the rotational speed was 1 rpm. Reference samples comprising extruded 134 sheets of PP containing the nucleating agent and PP/EB without the nucleating agent were 135 also prepared under conditions identical to those described above.

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137 Measurements

Thermal analysis was conducted using a differential scanning calorimeter (DSC) (Perkin Elmer, DSC 8000) under a nitrogen atmosphere to avoid thermal-oxidative degradation. Samples weighing approximately 3 mg were sealed in aluminum pans. The melting and crystallization profiles were recorded at a heating rate of 10°C min<sup>-1</sup> and a cooling rate of 10°C min<sup>-1</sup>.

143 The temperature dependence of the dynamic tensile moduli of the extruded 144 sheets was measured between -80°C and 175°C using a dynamic mechanical analyzer 145 (UBM, Rheologel-E4000-DVE). The frequency was 10 Hz and the heating rate was 2°C 146 min<sup>-1</sup>. The extruded sheet was cut into small rectangular pieces, 5 mm wide and 20 mm 147 long, that were mounted between gauges with a distance of 10 mm. The measurements 148 were carried out on two types of sample to investigate the mechanical anisotropy: one 149 was cut parallel to the flow direction (the machine direction (MD) sample), and the other 150 was perpendicular to the flow direction (the transverse direction (TD) sample). In the case 151 of the MD sample, the direction of the applied oscillatory strain coincided with the flow 152 direction.

153 To analyze the orientation and crystalline form of the PP molecules, wide-angle 154 X-ray diffraction (WAXD) patterns were collected using a high-speed two-dimensional 155 X-ray detector (Rigaku, PILATUS 3R 100K). The measurements were carried out using 156 CuKa radiation operated at 40 kV and 30 mA with a scanning range of 20 (the Bragg 157 angle) from 10° to 30°. Small pieces of the sample (approximately 1.0 mm thick) were 158 mounted on the diffractometer. The X-ray beam was irradiated normal to the MD-ND 159 plane (edge view: EV) and the MD-TD plane (through view: TV). For the EV 160 measurements, ten sheets of the sample were laminated with polystyrene solution, whereas only one sheet was used for the TV measurements. 161

162 The orientation of the PP lamellae was investigated using a transmission electron 163 microscopy (TEM) (JEOL, JEM-2100FX) at an acceleration voltage of 200 kV. The 164 samples were embedded in epoxy resin and sectioned using an ultramicrotome (RMC-165 Boeckeler, Ultramicrotome MT-XL) equipped with a diamond knife after exposure to the 166 vapor of ruthenium tetraoxide at 40°C for a day. Cross-sectional specimens (100 nm 167 thick) were cut from the stained sample in the MD-ND plane. 168 The deformation of the EB dispersed phase was observed by means of a scanning 169 electron microscopy (SEM) (Hitachi, S4100) with an acceleration voltage of 20 kV. For 170 non-conductive samples, the specimens were coated with Pt/Pd alloy for 60 seconds by 171 an ion sputtering machine (Hitachi, E1010). The surface of specimen was removed using 172 a rotary microtome (Yamato Kohki Industrial, RX-860) and immersed in xylene at room 173 temperature for 3 days to elute the rubber particles.

174 Stress-strain curves were investigated at room temperature using a tensile 175 machine (Tokyo Testing Machine, LSC-05/300) following ASTM D638. The specimens 176 were cut into dumbbell-shaped pieces (10 mm wide and 40 mm long) using dumbbell 177 cutter No.3 referenced from JIS K6251, in which the sample size was reduced by 40%. 178 The initial distance between the gauges was 30 mm, and one of the crossheads was moved up at a constant speed of 10 mm min<sup>-1</sup>. Stretching was performed in two directions: one 179 180 was parallel to the flow direction (the machine direction (MD) sample) and the other was 181 perpendicular to the flow direction (the transverse direction (TD) sample). All 182 measurements were performed at least five times, and the average values were calculated. 183 The elongation at break was evaluated by measuring the final gauge length of the narrow 184 part of the dumbbell.

185 The tear test was investigated by the Trouser method using a tensile machine 186 (Tokyo Testing Machine, LSC-05/300). Two types of sample were cut from the extruded 187 sheet; one had a notch parallel to the flow direction, that is, the machine direction (MD), 188 and the other had a vertical notch, that is, the transverse direction (TD). The specimens 189 were stretched at room temperature at a speed of 200 mm min<sup>-1</sup>. The distance between 190 the gauges was 20 mm.

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#### **Results and Discussion**

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### 194 Characterization of blend sheets

195 The melting and crystallization behaviors of the extruded sheets are shown in 196 Fig. 1. As shown in Fig. 1a, the pure PP sheet exhibits a main melting peak at 165°C, 197 suggesting  $\alpha$ -form crystals with a small shoulder peak of  $\beta$ -form crystals at 150°C. A 198 similar melting profile is observed in the PP/EB sheet. For the sheet containing the 199 nucleating agent, two distinct peaks are detected at 145°C and 151°C, which can be 200 attributed to  $\beta$ -form crystals. Furthermore, a sharp peak due to the  $\alpha$ -form crystals appears 201 at a slightly higher temperature than that for pure PP. The recrystallization after melting 202 of thick  $\beta$ -form crystals is responsible for thick lamellae of  $\alpha$ -form crystals leading to the 203 enhanced melting point as explained by Phulkerd et al. [29]. The same phenomenon is 204 observed for the PP/EB sheet containing the nucleating agent. Under suitable cooling 205 conditions, an annealed sheet of PP containing the nucleating agent has a melting point 206 due to  $\alpha$ -form crystals nearly at 170°C [29].

The crystallization behavior during the cooling process from 200°C is shown in Fig. 1b. There is no significant difference in the exothermic crystallization temperature (ca. 117°C) between the pure PP and PP/EB sheets. After the addition of the nucleating agent, the crystallization peak shifts to a higher temperature at 128°C in both the PP and PP/EB sheets. In this experiment, the crystallization temperature of PP is barely affected by EB irrespective of the addition of the nucleating agent, which also indicates that EB particles hardly affect the nucleating ability of the nucleating agent.

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216	Fig. 2 shows the X-ray diffraction curves in the equatorial direction of the MD-
217	TD plane, which are transformed and corrected using Lorentz and polarization (Lp)
218	factors. Both $\alpha$ - and $\beta$ -form crystals are detected but the $\beta$ -form crystals are predominant
219	in the sheets containing the nucleating agent. In the sheets without the nucleating agent,
220	the strong peak ascribed to the $\alpha$ -form crystals are detected, although $\beta(110)$ and $\beta(111)$
221	peaks are still confirmed. Relatively high cooling temperature (the chill roll was
222	maintained at 103°C) induces the $\beta$ -form crystallization to some extent. The XRD
223	patterns also suggest that the addition of EB to PP has a negligible effect on crystal
224	formation. Furthermore, there is an indication that the crystallinity of EB is significantly
225	low in the extruded sheets, because both (110) and (200) planes, which are attributable to
226	polyethylene crystals, are absent.
227	
228	[Fig. 2]
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230	Fig. 3 shows the 2D-WAXD patterns of the extruded sheets, obtained by
231	directing the X-ray beam in the normal direction for the edge view and in the transverse
232	direction for the through view. The $\alpha$ -form crystals in the pure PP show weak orientation,
233	as seen in Fig. 3a. The diffraction patterns of the PP/EB sheet (Fig. 3b) are almost
234	identical to those of the PP sheet, in which a diffraction peak attributed to the (040) plane
235	of the $\alpha$ -form crystals is detected in the equatorial direction, demonstrating that the PP
236	molecular chains are oriented in the MD direction. For the PP sheet containing the
237	nucleating agent (Fig. 3c), the PP chains in the $\beta$ -form crystals were oriented in the TD
238	direction. Such molecular orientation is also detected in the PP/EB sheet containing the

240	are observed as shown in Fig. 3d. This result demonstrates that PP chains preferentially
241	orient perpendicular to the flow direction. It also indicates that the nucleating agent
242	promotes the growth of $\beta$ -form crystals with the TD orientation of the PP molecular chains,
243	irrespective of the presence of EB.
244	
245	[Fig. 3]
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247	Fig. 4 shows a TEM image of a thin slice of the TD-ND plane cut from the PP/EB
248	sheet containing the nucleating agent. Phase-separated morphology is clearly seen in this
249	sample, in which the dark region is the EB phase. Furthermore, the crystalline lamellae
250	of PP are detected in the matrix as white lines, which preferentially orient along the ND.
251	Therefore, the growth direction of the PP chains is perpendicular to the ND, i.e., the TD
252	orientation, which corresponds well with the XRD patterns. The compressed stress
253	applied during the chill roll process is responsible for the preferential TD orientation of
254	PP chains, not the ND orientation. The slight deformation of EB particles to the TD would
255	be also attributed to the compression stress at the chill roll, although the deformation of
256	EB particles will be explained in detail later. Furthermore, PP lamellae are incorporated
257	into EB phase, which will provide the strong adhesion between them. This phenomenon
258	is attributed to the low interfacial tension between PP and EB, leading to large interphase
259	thickness in the molten state.
260	
261	[Fig. 4]
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263

Fig. 5 shows SEM images for the PP/EB sheet containing the nucleating agent.

264	The dark regions are attributable to the elongated pores formed by elution of the EB
265	particles with xylene. As seen in Fig. 5a, the numerous pores are mainly deformed in the
266	flow direction. The length of the pores is found to be approximately 3.0 $\mu m$ and the
267	diameter is about 0.5 $\mu$ m. On the other hand, a slight deformation in the TD direction with
268	an averaged pore size of 1.0 $\mu$ m for the length and 0.5 $\mu$ m for the diameter is detected in
269	the TD-ND plane, owing to the pressure applied by the chill roll, which corresponds with
270	the TEM image. The marked difference in the pore size between the MD and TD
271	directions demonstrates that EB preferentially orients in the flow direction. This is
272	understandable because the elongational stress in the air gap as well as the shear stress in
273	the die deform the EB particles in the flow direction by the hydrodynamic force. Similar
274	SEM images were obtained for the PP/EB sheet without the nucleating agent (but they
275	are not presented here). This suggests that the nucleating agent hardly affects the rubber
276	dispersion and deformation.
277	
278	[Fig. 5]
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280	Mechanical properties
281	Because the molecular orientation of PP is different from that of EB, the sample
282	sheet exhibits anomalous mechanical properties. Fig. 6 shows the dynamic mechanical
283	properties of extruded sheets employing two specimens to apply the oscillatory stain in
284	the different directions, i.e., the machine direction (MD) and transverse direction (TD).
285	As seen in Fig. 6a, both the MD and TD samples for the pure PP sheet show almost the
286	same dynamic tensile moduli over the whole range of temperature. A similar behavior is
287	also detected in the PP/EB sheet, in which PP molecules orient to the flow direction. Since

288 the molecular orientation is weak, no obvious mechanical anisotropy is observed for the 289 sample sheets without the nucleating agent. Moreover, E' in PP/EB falls off markedly 290 around 165°C which is attributed to melting of α-form crystals. For the PP sheet 291 containing the nucleating agent, in contrast, E' in TD is higher than that in MD at low 292 temperatures and vice versa at high temperatures. Based on the mechanical model 293 proposed by Takayanagi et al. [40], the anisotropy of the tie chain fractions, which are 294 deformed in the flow direction by hydrodynamic force during extrusion, is responsible 295 for the crossing behavior in the sample containing the nucleating agent [33]. A similar 296 mechanical behavior is detected for the PP/EB sheet containing the nucleating agent, 297 albeit the crossing behavior is weaker and shifted to the lower temperature region. As 298 compared with the PP/EB sheet, the addition of the nucleating agent enhances E' for the 299 MD sample over a wide temperature range above the glass transition  $(T_g)$ , owing to a high 300 degree of crystallinity resulting from the nucleating effect. Furthermore, a sharp drop of 301 *E'* is detected around 150°C due to the melting of the  $\beta$ -form crystals, which corresponds 302 to the DSC and WAXD results. It is found from Fig. 6b that both the PP/EB sheets with 303 or without the nucleating agent exhibit double peaks in the E" curve in the temperature range from -75°C to 40°C; the peak at the higher temperature is attributed to  $T_g$  of PP and 304 305 the other at the lower one is to that of EB.

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The stress-strain curves at the strain rate of  $0.006 \text{ s}^{-1}$  are shown in Fig. 7. The tensile force is applied along the MD or the TD. The difference in the tensile behavior between stretching in the MD and TD is detected in all samples. As seen in Fig. 7a, the

[Fig. 6]

312 pure PP sheet experiences a brittle fracture in the TD stretching beyond the yield point. 313 In the case of MD stretching, however, ductile deformation occurs under a low yield 314 stress. The PP containing the nucleating agent (Fig. 7b) shows high Young's modulus, 315 which corresponds to the tensile storage modulus. Moreover, yield stress in the MD 316 stretching is greatly enhanced with a ductile manner. The low modulus of EB is 317 responsible for marked decrease in Young's modulus and yield stress for both the PP/EB 318 and PP/EB containing the nucleating agent as seen in Figs. 7c and 7d. In the PP/EB sheet 319 containing the nucleating agent, the anisotropy in Young's modulus and yield stress is 320 considerably weaker than that in the PP sheet containing the nucleating agent. The strain 321 at break in the TD stretching for PP containing the nucleating agent is considerably larger 322 than that for pure PP. The ductile behavior is also observed in MD stretching, although 323 the yield stress is high. As a result, the anisotropy of strain at break becomes reduced 324 following the addition of the nucleating agent. The reduction of the mechanical anisotropy 325 becomes more apparent for the blend containing EB, although it is interesting to note that 326 the PP/EB exhibits ductile behavior not only in MD but also in TD stretching. Since the 327 yield stress in TD stretching is lower than that in MD stretching, the deformation of EB 328 particles into flow direction affects the stress-strain behavior greatly, although the 329 deformation behavior of the EB phase is not revealed in this study. The details of 330 mechanical anisotropy in terms of crack propagation are discussed below.

- 331
- 332

[Fig. 7]

333

334 Trouser tear test was carried out at room temperature employing two types of the 335 sheet samples; one has a parallel notch in the flow direction (MD), and the other has a

336	vertical notch (TD). As seen in Fig. 8a, the pure PP sheet shows higher tear strength in
337	the TD sample. For PP containing the nucleating agent (Fig. 8b), the order is opposite
338	with an enhanced anisotropy in tear strength. In the case of the blend, the tear strength in
339	the TD sample is markedly enhanced, irrespective of the nucleating agent. Furthermore,
340	the direction of crack propagation changes to the MD immediately after the stretching as
341	demonstrated in Figs. 8c and 8d. These results demonstrate that PP orientation has no
342	marked impact on the tear property. The deformation of EB particles plays a dominant
343	role on the tearing. Such information has never been reported before to the best of our
344	knowledge, because the deformation direction of a dispersion is always the same as the
345	molecular orientation direction of matrix in general. Regarding the effect of the nucleating
346	agent, the tear strength of the MD sample is slightly enhanced, although the effect is not
347	as obvious as in the pure PP.
348	
349	[Fig. 8]
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352	Conclusions
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354	An extruded sheet with unique structure was developed using a blend comprising
355	PP, EB, and a small amount of N,N'-dicyclohexyl-2,6-naphthalenedicarboxamide. It was
356	found that the nucleating agent promotes the formation of $\beta$ -form crystals and causes the
357	PP chains orient perpendicular to the flow direction in an extruded sheet, i.e., in the
358	transverse direction, as confirmed by 2D-XRD and TEM characterization. On the contrary,

360	orientation of the PP molecules is perpendicular to the deformation direction of the EB	
361	droplets, which affects the mechanical anisotropy to a great extent. With regard to the	
362	tensile properties, the anisotropy in yield stress and strain at break is significantly	
363	decreased owing to this peculiar structure. It is proved by the tear test that the strength of	
364	the TD sample is increased with a crack growth in the flow direction. This result	
365	demonstrates that the deformation of the EB particles in the MD direction exhibits more	
366	pronounced effect than the molecular orientation of the PP chains in the TD direction.	
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(a)

(b)



Fig. 1 DSC profiles of extruded sheets; (a) heating curves and (b) cooling curves.



Fig. 2 Lp-corrected XRD curves obtained from the through view beam for extruded sheets.



Fig. 3 WAXD patterns of the edge views (MD-ND) and the through views (MD-TD) in the samples; (a) PP, (b) PP/EB, (c) PP containing the nucleating agent, and (d) PP/EB containing the nucleating agent.



Fig. 4 TEM image of the TD-ND plane ( $\times$ 15,000) for PP/EB containing the nucleating agent.



Fig. 5 SEM images of PP/EB containing the nucleating agent. (a) MD-ND plane and (b) TD-ND plane.



Fig. 6 Temperature dependence of dynamic tensile modulus of extruded sheets at 10 Hz; (a) tensile storage modulus *E*' and (b) tensile loss modulus *E*''. The applied strain was (grey symbol) parallel to the flow direction (MD) and (black symbol) perpendicular to the flow direction (TD).



Fig. 7 Stress-strain curves of (a) PP, (b) PP containing the nucleating agent, (c) PP/EB, and (d) PP/EB containing the nucleating agent at a strain rate of 0.006 s<sup>-1</sup>.



Fig. 8 Tear-propagation resistance (TPR) versus the applied displacement of notched specimens in MD and TD directions; (a) PP, (b) PP containing the nucleating agent, (c) PP/EB, and (d) PP/EB containing the nucleating agent.